

Q - Refrigerant R₂₂ enters a well-insulated compressor at 3.5 bar, -5°C and exits at 14 bar. Determine the work input in kJ/kg if the outlet temperature 75°C.
($\gamma = C_p/C_v$ for R₂₂ is 1.562 at -5°C and 1.348 at 75°C)

Given $\gamma = C_p/C_v$ at -5°C = 1.562

$$\text{Hence } C_p \text{ (at } -5^\circ\text{C)} = \frac{\gamma R}{\gamma - 1} = 2.90 * R = 2.90 * 8.31 = \mathbf{24.11 \frac{J}{mol.K}}$$

And $\gamma = C_p/C_v$ at 75°C = 1.348

$$\text{Hence } C_p \text{ (at } 75^\circ\text{C)} = \frac{\gamma R}{\gamma - 1} = 3.87 * R = 3.87 * 8.31 = \mathbf{32.19 \frac{J}{mol.K}}$$

If we consider a controlled volume of air in the compressor, and the steady state then the total change of internal energy inside the compressor will be zero and we can write

$$H_{in} - H_{out} + W_{in} = 0 \quad \text{----- (1)}$$

Here

H_{in} = Enthalpy (or heat content) entering the compressor with input air.

H_{out} = Enthalpy coming out of the compressor with output air.

W_{in} = Work going in as the power input.

Let n mol of R₂₂ flows through the compressor per second.

As the enthalpy is given by

$$H = U + PV = n * C_v * T + n RT \quad [PV = n RT]$$

$$\text{Or } H = n (C_v + R) T = n C_p T$$

Here C_v and C_p are the molar specific heats of R₂₂ at constant volume and constant pressure respectively

Thus the input and output enthalpy is given by

$$H_{in} = n C_p T_1 = n * (24.11 \text{ J.mol}^{-1}.\text{K}^{-1}) * (273 - 5) \text{K} = n * 6.46 \text{ KJ}$$

$$H_{out} = n C_p T_2 = n * (32.19 \text{ J.g}^{-1}.\text{K}^{-1}) * (273 + 75) \text{K} = n * 11.20 \text{ KJ}$$

Substituting above in equation (1) we get

$$H_{in} - H_{out} + W_{in} = 0$$

$$\text{Or } n * 6.46 - n * 11.20 + W_{in} = 0$$

$$\text{Or } W_{in} = n * 4.74 \text{ KJ}$$

As the molecular weight of CHClF₂ is 86.48 g/mol, 1 kg of R₂₂ will have

$$1000 / 86.48 = 11.56 \text{ mol and hence we get}$$

$$W_{in} = 11.56 * 4.74 = 54.8 \text{ KJ/Kg}$$